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Serial No. 10/753,300
Docket No. S00033 US NA

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AMENDMENTS TO THE CLAIMS

1. (Canceled)
2. (Canceled)
3. (Canceled)
4. (Canceled)
5. (Canceled)
6. (Canceled)
7. (Canceled)
8. (Currently Amended) The process of claim ± 47, wherein the melt viscosity is from about 500 to about 700 Pascals at 250°C and 48.65 per second shear rate.
9. (Canceled)
10. (Canceled)
11. (Currently Amended) The process of claim ± 47, wherein the filament denier is at least 15.
12. (Canceled)
13. (Canceled)
14. (Currently Amended) The process of claim 56 47, wherein the yarn denier is at least 1000.
15. (Canceled)
16. (Canceled)
17. (Canceled)
18. (Canceled)

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19. (Canceled)

20. (Currently Amended) The process of claim ~~4~~ 47, further comprising coating the filaments with a spin finish and optionally preintermingling the filaments.

21. (Canceled)

22. (Canceled)

23. (Currently Amended) The process of claim ~~4~~ 47, wherein the bulking the drawn filaments is to form 3-dimensional curvilinear crimp therein.

24. (Original) The process of claim 23, wherein the bulking comprises blowing and deforming the filaments in a hot-fluid jet bulking unit.

25. (Canceled)

26. (Previously Presented) The process of claim 47, wherein the draw ratio is about 1.2 to about 3.0.

27. (Canceled)

28. (Canceled)

29. (Twice Amended) The process of claim ~~4~~ 47, wherein the intrinsic viscosity is about 0.98 to about 1.04.

30. (Canceled)

31. (Canceled)

32. (Canceled)

33. (Currently Amended) The process of claim ~~34~~ 47, wherein the water content is less than about 40 ppm.

34. (Canceled)

35. (Canceled)

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36. (Canceled)

37. (Canceled)

38. (Canceled)

39. (Canceled)

40. (Canceled)

41. (Currently Amended) The process of claim ~~31~~ 47, further comprising ply-twisting and heat setting the filaments into yarn.

42. (Original) Carpet made from the ply-twisted, heat-set poly(trimethylene terephthalate) yarn of claim 41.

43. (Canceled)

44. (Canceled)

45. (Canceled)

46. (Currently Amended) The process of claim ~~1~~ 47, wherein the process further comprises providing poly(trimethylene terephthalate) chip and drying the poly(trimethylene terephthalate) chip at about 80 to about 150°C.

47. (Currently Amended) A process of forming poly(trimethylene terephthalate) bulk continuous filament yarn comprising:

a. providing poly(trimethylene terephthalate) chip wherein the poly(trimethylene terephthalate) has a number average molecular weight of about 26500 29000 to about 40000, an intrinsic viscosity of about 0.95 to about 1.04 dl/g, and a melt viscosity of about 450 350 up to about 700 Pascals at 250°C and 48.65 per second shear rate,

b. drying the poly(trimethylene terephthalate) chip to a water content of less than about 50 ppm,

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- c. melting the poly(trimethylene terephthalate) chip in a single screw extruder,
- d. extruding the poly(trimethylene terephthalate) to form filaments;
- e. cooling the filaments,
- f. converging the filaments into yarn;
- g. drawing the filaments at a speed of greater than 3000 3500 meters per minute, at a draw ratio of about 1.1 to about 4.0, to produce filaments having a filament denier greater than 10 and yarn having a yarn denier greater than 210 of at least 500;
- h. bulking the drawn filaments;
- i. cooling the bulked filaments through a cooling drum,
- j. intermingling the cooled filaments, and
- k. winding the intermingled filaments on a wind-up machine.

48. (Previously Presented) The process of claim 47 wherein the bulking the drawn filaments is carried out using a bulking unit with a texturing nozzle.

49. (Canceled)

50. (Previously Presented) The process of claim 47, wherein the filaments are drawn at a speed of greater than 4000 meters per minute.

51. (Previously Presented) The process of claim 47, wherein the filaments are drawn at a speed of greater than 3500 meters per minute up to less than 5000 m/min.

52. (Previously Presented) The process of claim 47, wherein the draw ratio is about 1.4 to about 2.2.

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53. (Previously Presented) The process of claim 47, wherein the intrinsic viscosity is about 1.00 to about 1.02 dl/g.

54. (Previously Presented) The process of claim 47, wherein the intrinsic viscosity is about 0.95 to about 1.02 dl/g.

55. (Canceled)

56. (Canceled)